

**CLAIM AMENDMENTS**

Amend claims: 1-10 and added new claims 11-18.

1. (Currently Amended) A process ~~Process~~ to prepare a base oil having a target viscosity index of above 80 and a saturates content of above 90 wt% from a crude derived feedstock ~~by comprising~~
  - (a) contacting a crude derived feedstock in the presence of hydrogen with a catalyst comprising at least one Group VIB metal component and at least one non-noble Group VIII metal component supported on a refractory oxide carrier to produce an effluent;
  - (b) adding to the effluent of step (a) or part of the effluent of step (a) a Fischer-Tropsch-derived fraction boiling at least partly in the base oil range, wherein the Fischer-Tropsch derived fraction is obtained by hydroisomerization of a Fischer-Tropsch synthesis product, in an amount effective to achieve the target viscosity index of the final base oil to produce a mixture; and
  - (c) dewaxing the mixture as obtained in step (b).
2. (Currently Amended) The process of ~~Process~~ according to claim 1, wherein the crude derived feedstock is a vacuum distillate fraction or a de-asphalting vacuum residue as obtained from ~~the residue of the~~ an atmospheric distillation of a crude petroleum feed.
3. (Currently Amended) The process of ~~Process~~ according to any one of claims 1-2, wherein the viscosity index of the crude derived feedstock is below 60.
4. (Currently Amended) The process of ~~Process~~ according to any one of claims 1-3, wherein the conversion in step (a) is between 20 and 80 wt%.
5. (Currently Amended) The process of ~~Process~~ according to any one of claims 1[[-4]], wherein in step (a) the crude derived feedstock is first subjected to a hydrotreating step prior to the hydrocracking step.

6. (Currently Amended) The process of Process according to claim 5, wherein the conversion in the hydrotreating step is below 30 wt%.

7. (Currently Amended) The process Process according to any one of claims 1-6, wherein the kinematic viscosity at 100 °C of the mixture as obtained in step (b) is between 3 and 10 cSt.

8. (Currently Amended) The process Process according to any one of claims 1-7, wherein step (c) comprises is performed by means of catalytic dewaxing.

9. (Currently Amended) The process Process according to any one of claims 1-8, wherein the dewaxed product of step (c) is subjected to an additional hydrogenation treatment step (d).

10. (Currently Amended) The process Process according to any one of claims 1-9, wherein the Fischer-Tropsch derived fraction is a partly isomerized isomerised Fischer-Tropsch fraction boiling for more than 90 wt% above 300 °C, having a congealing point below 80 °C and a wax content of below 50 wt%.

11. (New) The process of claim 2, wherein the viscosity index of the crude derived feedstock is below 60.

12. (New) The process of claim 2, wherein the conversion in step (a) is between 20 and 80 wt%.

13. (New) The process of claim 2, wherein in step (a) the crude derived feedstock is first subjected to a hydrotreating step prior to the hydrocracking step.

14. (New) The process of claim 13, wherein the conversion in the hydrotreating step is below 30 wt%.

15. (New) The process of claim 2, wherein the kinematic viscosity at 100 °C of the mixture as obtained in step (b) is between 3 and 10 cSt.
16. (New) The process of claim 2, wherein step (c) comprises is performed by means of catalytic dewaxing.
17. (New) The process of claim 2, wherein the dewaxed product of step (c) is subjected to an additional hydrogenation treatment step (d).
18. (New) The process of claim 2, wherein the Fischer-Tropsch derived fraction is a partly isomerized fraction boiling for more than 90 wt% above 300 °C, having a congealing point below 80 °C and a wax content of below 50 wt%.